

**SPRING21
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The diagram shows two safety logic configurations:

- Median Select (or mid-value) Select for 3 control sensors:** This configuration uses three BPCS Sensors (1, 2, 3) connected to a Median Select logic block. The output of the logic block is connected to a Positioner, which then controls a BPCS Valve.
- 2oo3 voting for safety sensors:** This configuration uses three SIF Sensors (SA, SB, SC) connected to a 2oo3 Voting logic block. The output of the logic block is connected to a SIF Solenoid Valve (SIF Valve A). A second SIF Solenoid Valve (SIF Valve B) is also shown, connected to an Instr. Air Supply and a Vent.

- **Median (or mid-value)**
Select for 3 control sensors
- Reduced trips from transmitters that drift or that have bad PV
- **2oo3 voting** for safety sensors
- Reduced spurious trips
- Lower PFD than 1oo1 voting

- 3 sensors working – **dark blue**
- 1 sensor failed, drift (dangerous detected or dangerous undetected), bad PV (detected) – **light blue** – control & SIF are still functional
- Unavailability states with 2 or 3 sensors failed. – **light red**
- Tripped states – **light green**

- Based on failure rates (and number of sensors that have not yet failed) and repair rate.
 - Sensor failure rate, $\lambda = 1.67\text{E-}2/\text{year}$
 - DD Drift, $\delta\delta = 0.8 * \lambda = 1.34\text{E-}2/\text{yr.}$
 - DU Drift, $\delta v = 0.1 * \lambda = 1.67\text{E-}3/\text{yr.}$
 - Bad PV, $\beta\pi\omega = 0.1 * \lambda = 1.67\text{E-}3/\text{yr.}$
 - Repair rate, $\mu = 121.67/\text{yr.}$
(72 hr. MTTR)
 - Proof Test Interval = 1 year

The diagram illustrates the SIF control system architecture. It begins with BPCS Sensors (1, 2, 3) providing input to a Median Select or Mid-Value Select block. This block's output goes to a Zoo3 Voting block, which also receives inputs from a Ringbus and a CPU. The Zoo3 Voting block outputs to a Positioner (I/P) block. The Positioner controls a BPCS Control Valve, which is part of a SIF Solenoid Valves assembly. This assembly includes Instr. Air Supply, Vent, and SIF Valve A and B. The SIF Solenoid Valves assembly is controlled by a SIF Solenoid Valve block, which also receives inputs from the BPCS Control Valve and the Positioner.

Diagram illustrating the 2003 Voting process:

- SIF Sensors & BPCS Sensors** (A, B, C) provide input to the **Median Select or Mid-Value Select** process.
- The **Median Select or Mid-Value Select** process outputs to the **BPCS** (Basic Process Control System).
- The **BPCS** outputs to the **SIF** (Safety Instrumented Function) system.
- The **SIF** system includes **Sensor**, **Buffer**, and **Voter** components.
- The **SIF** system outputs to the **2003 Voting** process.

- Fault Tree Analysis could be used, but it is difficult to model failure modes and failure sequences in time.
- Markov models can handle different failure modes and failure sequences in time.
- A **Markov model** was used [3].
- For simplicity, the model was limited to the sensors configuration.

○ = unavailability state

Mean unavailability states (PFD) = 5.6E-4

- For 2oo3 sensor voting, the Probability of Failure on Demand (PFD) is $5.62\text{E-}4$. **This is a reasonable value for the sensor part of an SIF.**
- For median select or mid-value select for control sensors, the expression $\text{PFD} = \lambda T/2$ is solved for λ . For a 1 year test interval, **the failure rate, λ , for the control sensors is $1.12\text{E-}3/\text{yr}$, an order of magnitude lower than the single sensor failure rate of $1.67\text{E-}2/\text{yr}$.**

- If the **SIF trips** on the 2003 sensors, the BPCS control loop shall be automatically placed in **manual** and the output to the valve shall be **set to 0**. Required to avoid a “race” condition in which the control loop sees a 0 PV and attempts to open the control valve.
- The **loops** for each of the three sensors shall be **powered by the SIF logic solver**.
- There are **other schemes** to share process variables between the SIF and the BPCS but analysis of their failure modes is **beyond the scope** of this paper.
- Provision should be made for the BPCS to **calculate the mean value correctly** when the **sensors are in a degraded state**
 - 1 sensor with bad PV (detected)
 - 1 sensor drifted (detected)
- It is critical that **detected failures be repaired within 72 hours**.
- **Future work:** include more explanation for human factors that introduce errors during testing [4].

1. IEC 61511-1:2016+AMD1:2017 CSV, Consolidated version: Functional Safety – Safety instrumented systems for the process industry sector - Part 1: Framework, definitions, system, hardware and application programming requirements, International Electrotechnical Commission (IEC), 2010, Geneva, Switzerland.
2. ANSI/ISA-61511-1-2018 / IEC 61511-1:2016+AMD1:2017 CSV, Functional Safety – Safety Instrumented Systems for the Process Industry Sector – Part 1: Framework, definitions, system, hardware and application programming requirements (IEC 61511-1:2016+AMD1:2017 CSV, IDT), International Society of Automation, Research Triangle Park, North Carolina.
3. CCPS, *Layer of Protection Analysis, Simplified Process Risk Assessment*, American Institute of Chemical Engineers, New York, New York, 2001.
4. ISA-TR84.00.02-2015, Safety Integrity Level Verification of Safety Instrumented Functions, Annex E, Markov Analysis. International Society of Automation, Research Triangle Park, North Carolina.
5. "SIL-3, SIL-2, and Unicorns (There is a High Probability Your SIL 2 and SIL 3 SIFs Have No Better Performance Than SIL 1)", A.M. (Art) Dowell, III, W. Bridges, M. Massello, and H.W. (Hal) Thomas, *15th Global Congress on Process Safety*, New Orleans, LA, AIChE, March 31-April 3, 2019

Acronym	Definition
1oo1	1 out of 1 voting
2oo3	2 out of 3 voting
BPCS	Basic Process Control System
βπω	Bad PV failure rate
CPU	Central Processing Unit (or Controller Card)
DD	Dangerous Detected
DU	Dangerous Detected
δδ	Drift dangerous detected failure rate
δu	Drift dangerous undetected failure rate
I/P	Current to pneumatic transducer
λ	Failure rate, per year
mA	Milliamperes
MTTR	Mean Time To detect and Repair, years. $1/MTTR = \mu$
μ	repair rate, per year
PFD	Probability of Failure on Demand
PV	Process Variable
SIF	Safety Instrumented Function
SIL	Safety Integrity Level

- The **Markov Model** Module in **Reliability Workbench 13.0.2.0** provided by **Isograph LTD.**



Art has a BA and BS in Chemical Engineering and has more than 50 years of process safety experience, including 42 years at Rohm & Haas; now The Dow Chemical Company. Art has published more than 50 papers, many on PHA, LOPA, and SIS implementation. PII has helped more than a hundred companies implement process safety since 2003. This includes leading hundreds of PHAs for both new projects and existing plants and training more than 4000 PHA leaders and scribes. PII staff has performed more than 1000 LOPA and more than 1000 SIL Verification.